

H = enthalpy
 P = pressure
 R = universal gas constant, 1.9872 B.t.u./lb.-mole \circ R.
 S = entropy
 T = temperature
 V = volume
 α = residual volume

Superscripts

$^\circ$ = zero pressure, ideal gas state
 * = unit fugacity, ideal gas state

Subscripts

c = critical constants
 L = liquid phase
 v = vapor phase

LITERATURE CITED

- (1) Bennewitz, K., Rossner, W., *Z. physik. Chem.* **B39**, 126 (1938).

- (2) Foz Gazulla, O.R., Morcillo, J., Mendez, A., *Anales real. soc. españ. fis. y quím. (Madrid)* **50B**, 17 (1954).
- (3) International Critical Tables, Vol. III, p. 218, Vol. V, p. 137, McGraw-Hill, New York, 1928.
- (4) Kobe, K.A., Harrison, R.H., Pennington, R.E., *Petrol. Refiner* **30**, No. 8, 119 (1951).
- (5) Lyderson, A.L., Greenkorn, A.R., Hougen, O.A., "Generalized Properties of Pure Fluids," Eng. Expt. Station, Univ. Wisconsin, Rept. 4 (October 1955).
- (6) Ramsey, William, Young, Sidney, *Phil. Trans. Roy. Soc. (London)* **180A**, 137 (1889).
- (7) Scarborough, J.B., "Numerical Mathematical Analysis," 4th ed., p. 128, Johns Hopkins Press, Baltimore, Md., 1958.
- (8) Sinke, G.C., De Vries, Thomas, *J. Am. Chem. Soc.* **75**, 1815 (1953).
- (9) Stull, D.R., *Ind. Eng. Chem.* **39**, 517 (1947).
- (10) Wylie, C.R., Jr., "Advanced Engineering Mathematics," p. 512, McGraw-Hill, New York, 1951.
- (11) Young, Sidney, *Z. physik. Chem.* **70**, 620 (1910).

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CORRECTION

In "Prediction of Equilibrium Ratios from Nomograms of Improved Accuracy" [B.C. Cajander, H.G. Hipkin, and J.M. Lenoir, *J. CHEM. ENG. DATA* **5**, 251 (1960)] the figures entitled "Equilibrium ratios of aliphatic hydrocarbons at 10 p.s.i.a." in the right column on page 254 are incorrect.

The line labeled butadiene-1,2 is low by about 30%. The line labeled 2 or 3-methylbutene-1 is correct for 3-methylbutene-1, but 2-methylbutene-1 should lie between pentene-1 and isoprene. The corrected figures appear as shown below.

